

is held at a minimum at any given time of the reaction to minimize the formation of homopolystyrene

REMARKS

In this case, claims 1-10 are currently under examination. Claim 3 has been amended to correct an inadvertent error in dependency, and Claim 7 has been amended to correct an error in naming. These amendments are not substantive, and do not narrow the claims. The claims are now considered to be in order for allowance.

Issue 1: Restriction (35 U.S.C. §121)

Applicants elect with traverse Claims 1-6 drawn to a resin composition. Applicants further elect with traverse a resin composition that has not been hydrogenated. Applicants respectfully submit that there will not be undue searching required for a resin composition whether it is hydrogenated or not, and requests that examination be conducted on both hydrogenated and non-hydrogenated resin compositions.


Issue 2: Indefiniteness Rejection (35 U.S.C. § 112)

Claims 3 and 7-10 are rejected under 35 U.S.C. § 112, second paragraph as indefinite as to scope. Claim 3 has been amended to depend from Claim 2, which refers to a partially hydrogenated resin composition. Claim 7 has also been amended to delete the term "recycled reactants", and replace it with "unconverted reactives". Support for the term "unconverted reactives" is found on page 13, line 22 of the disclosure.

Applicants believe that the amended claims are now allowable.

Respectfully submitted,

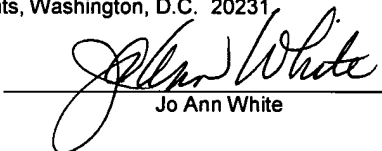
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I hereby certify that this paper (along with any paper(s) referred to as being attached or enclosed) is being deposited with the United States Postal Service with sufficient postage as first class mail in an envelope addressed to: Assistant Commissioner for Patents, Washington, D.C. 20231


Jo Ann White

December 10, 2002
Date

VERSION WITH MARKINGS TO SHOW CHANGES MADE**IN THE CLAIMS:**

Claim 3.(amended) The resin composition of Claim [1] 2, wherein hydrogenation of the olefin is about 95% or greater and hydrogenation of the aromatics is up to about 20%.

Claim 7. (amended) A process for producing an aromatic-modified DCPD resin having an M_z of less than about 2,000 comprising the steps of: (i) providing solvent or [recycled reactants] unconverted reactives to a reactor; (ii) heating said solvent or [recycled reactants] unconverted reactives to a temperature of about 200°C to about 265°C, and (iii) adding a monomer mixture comprising about 5 to about 25% by weight styrene in combination with about 75 to about 95% DCPD monomer, at a rate to consume styrene monomer at the rate at which it is added such that the concentration of free styrene monomers in the reaction medium is held at a minimum at any given time of the reaction to minimize the formation of homopolystyrene.